

# SteamDry

## Opportunities and challenges in superheated steam drying (SSD): A paper industry case



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**Joanne Siccama**

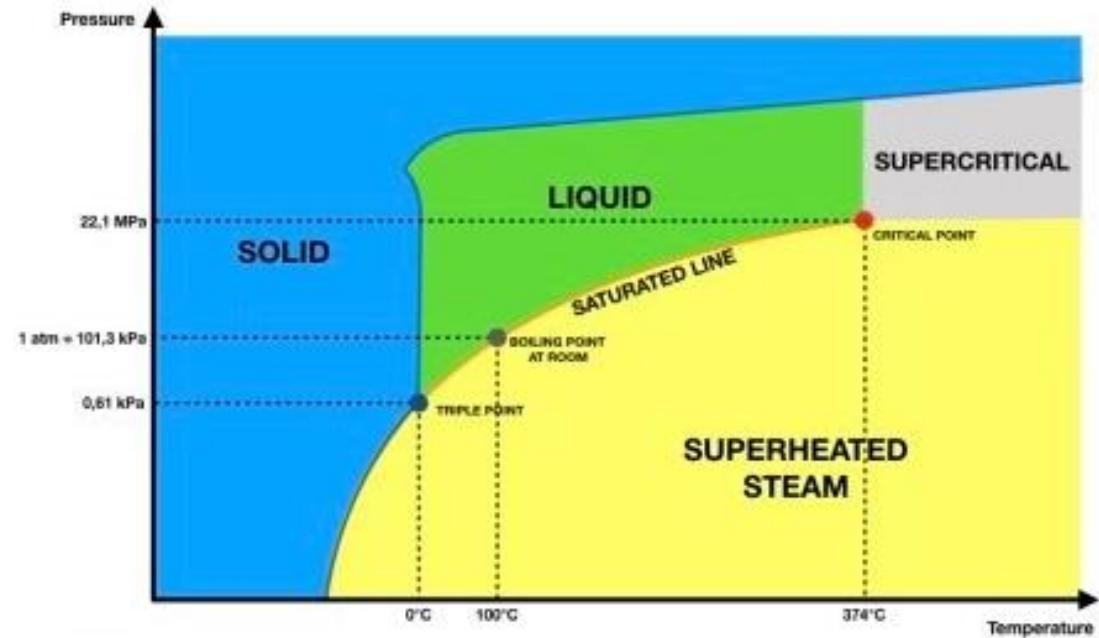
Wageningen Food & Biobased Research

# Outline

- Superheated steam drying (SSD)
  - Advantages
- Current applications
- Case: paper industry
  - Dryer concepts
  - Challenges to be solved
- Conclusions and Outlook

# Superheated steam drying (SSD)

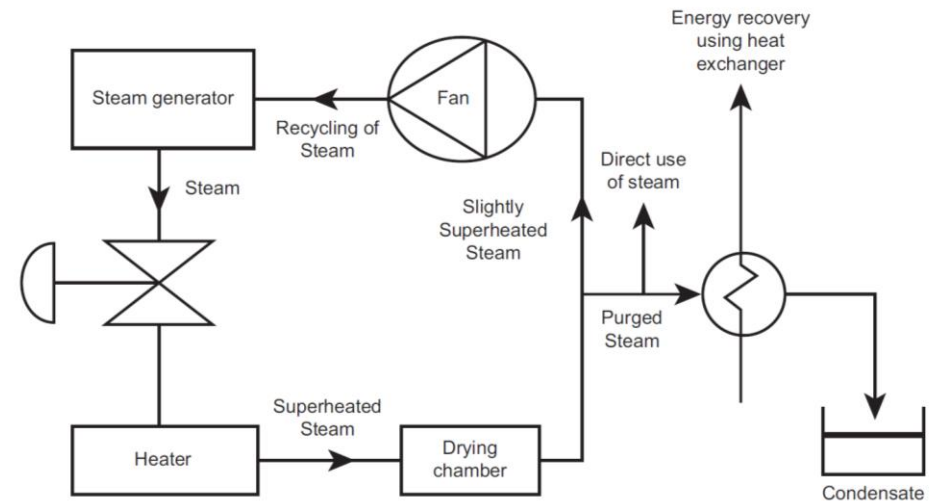
- Principle known for almost 100 years
- Definition superheated steam: “Steam at a temperature higher than its vaporization point at the absolute pressure where the temperature is measured”
- The steam is not saturated, hence water can be evaporated and become part of the steam
- Product temperature increases to the evaporation temperature



Palo, 2018

# Superheated steam drying (SSD)

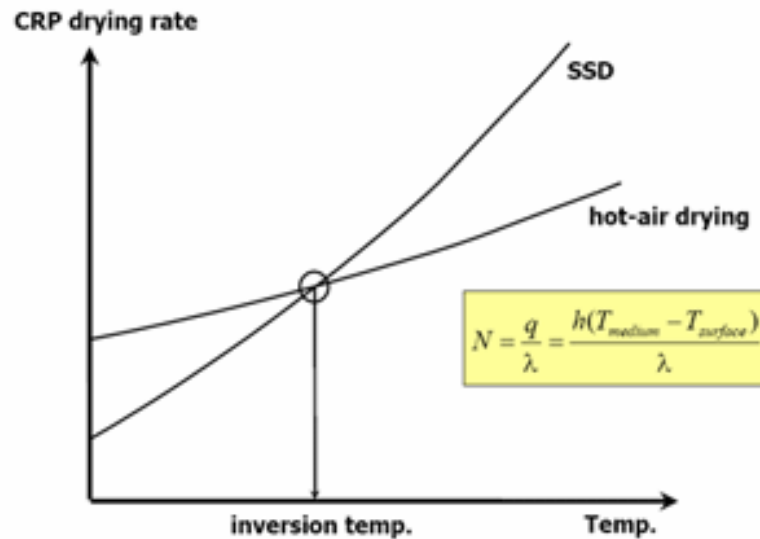
- Operation pressure determines the drying temperature
- Three sorts of dryers
  - Low pressure (5-30 kPa) – heat-sensitive products (fruit and vegetables)
  - Atmospheric pressure
  - High pressure (2-25 bar) – surplus steam more easily reused
- Net energy consumption can be as low as 700-1000 kJ/kg water evaporation (Mujumdar, 2007) → 10-20% of energy consumption air drying



Sehrawat et al., 2016

# Drying rates of SHS vs air

- Higher drying rates are possible for SHS in constant rate period (CRP) depending on steam temperature



Devahastin, 2008

- Thermal conductivity
- Heat capacity

- The inversion temperature depends on the flow conditions, more turbulence lowers the inversion temperature
- Typically, in the range of 160-350°C (equal mass flow steam and air)

- The drying rate in falling rate period is higher in SHS:
  - No resistance of moisture diffusion in its own vapour
  - No case-hardened skins (water-impermeable) are formed in SSD

# SSD - Advantages

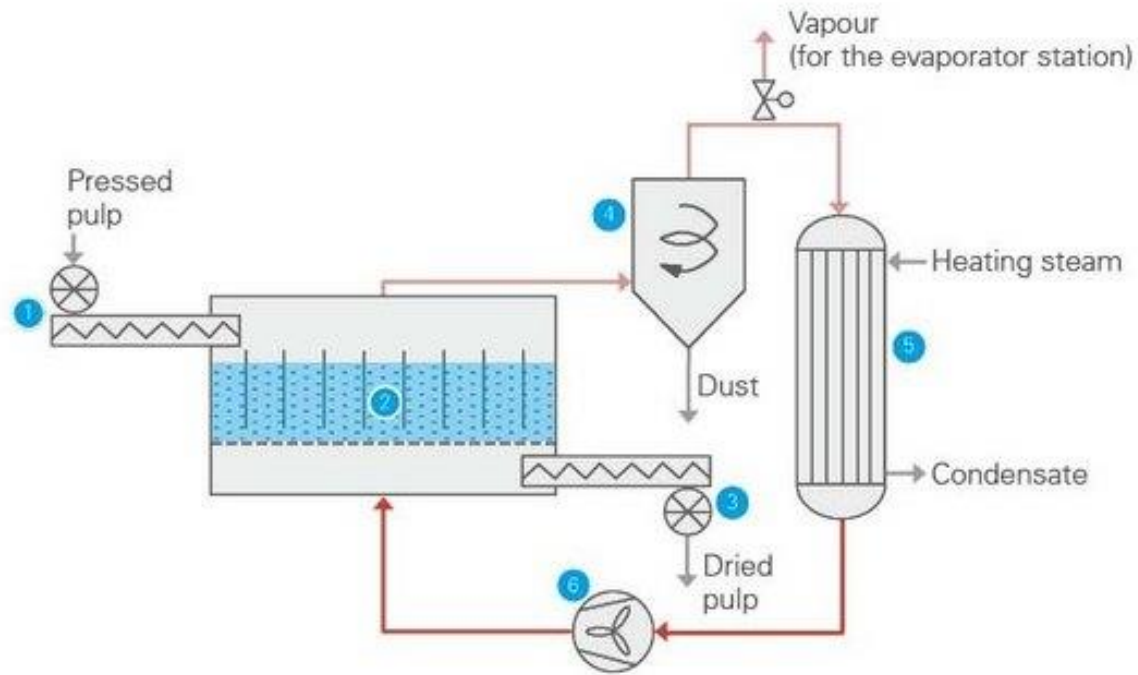
- Energy reduction → only when surplus steam is utilized!
- Easier to recover energy of SHS than from moist air
- Higher drying rate, when above the inversion temperature, compared with air  
→ smaller dryer
- No oxidation
- Minimum risk of fire or explosion
- Process can be fully electrified

# Current industrial applications

- Fluidized-bed drying of beet pulp (3-5 bar) – Cosun, the Netherlands (BMA)  
[Fluidised Bed Steam Dryer | Efficient drying solutions from BMA \(bma-worldwide.com\)](https://www.bma-worldwide.com)
- Fluidized-bed drying of pulverized lignite coal (atmospheric) – Coal Innovation Centre, Niederaussem (Germany) (RWE Power AG)  
<https://www.ispatguru.com/wta-technology-for-drying-of-lignite-coal/>

# Fluidized-bed drying of beet pulp

- Working principle:



- 1 Input
- 2 Cells and fluidised bed
- 3 Discharge
- 4 Dust separator<sup>1)</sup>
- 5 Heat exchanger
- 6 Fan
- Media
- Steam/vapour circulation

1) Dust separator with inlet openings exclusively in the lower part.

BMA, 2024



# Fluidized-bed drying of beet pulp

## Advantages:

- Efficient use of surplus steam in evaporator station → thereby reduce energy demand
- Lock technology BMA prevents minimum steam losses
- Reduction of odours → happy neighbours
- Nutrients in pressed pulp are largely preserved





# Fluidized-bed drying of pulverized lignite coal

Advantages for lignite coal drying:

- Large amounts of water needs to be removed
  - Input 210 tons/h raw lignite coal throughput
  - Evaporation capacity 100 tons/h
- Drying at inert atmosphere → ensure safety for the potentially explosive characteristics of dry lignite coal
- Drying temperature relatively low: evaporation at 110°C (slight overpressure)

# Case: paper industry - EU-project SteamDry

- Superheated steam drying for sustainable and recyclable web-like materials
- Develop drying technology that saves 60% of energy compared to BAT for tissue and board industry

	CURRENT	STEAMDRY
 ENERGY	~1100 kWh/ton	~450 kWh/ton
 CO2 (fossil)	0.45 tCO2/t paper	No emissions
 HEAT	30-40% lost to air	Latent heat recovered
 SOURCE	Combustion	Electricity



# Case: paper industry

- The process of paper making is a water and energy-intensive process

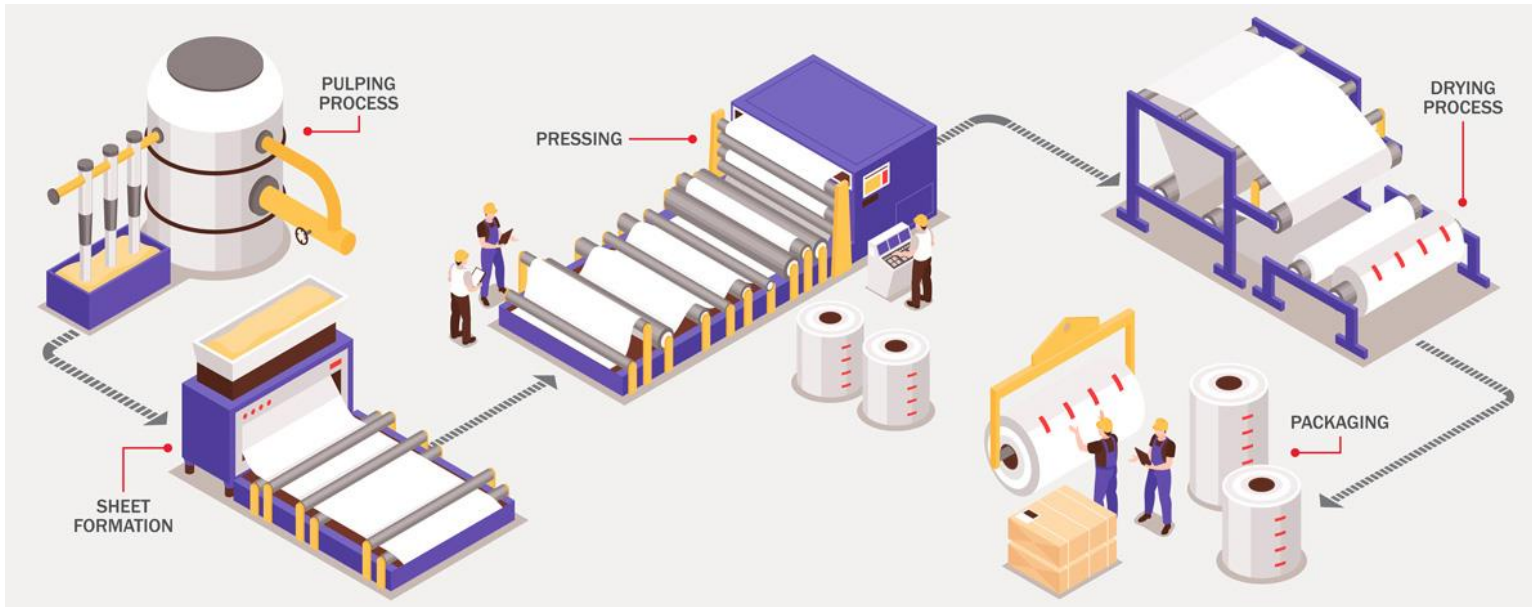


Image: Dwyer Instruments

# Case: paper industry

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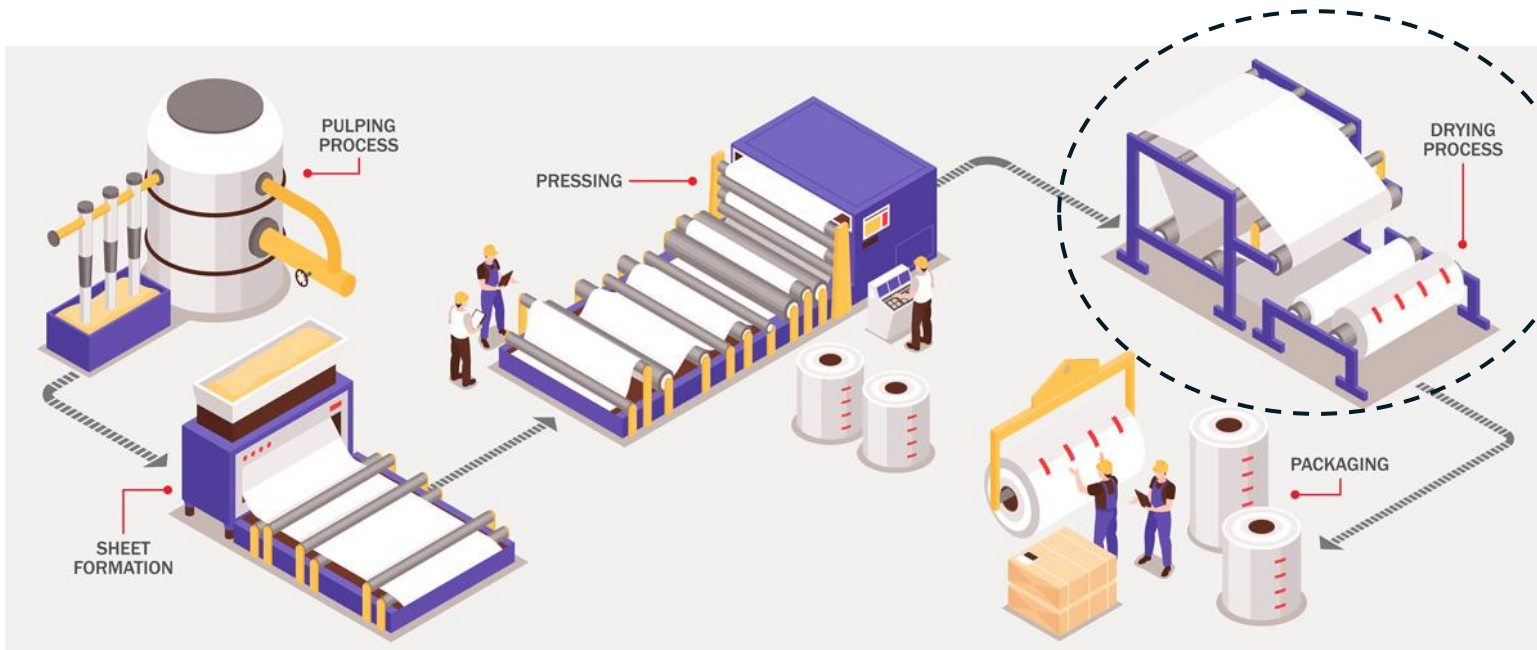


Image: Dwyer Instruments

# Drying process

- Input dryer (after press): 35-55% dry matter
- Output dryer: 95% dry matter
- Different dryer types are used:
  - Multicylinder dryers (conductive drying)
  - Impingement dryers (convective drying)
  - Yankee dryers → tissue industry
    - One large cylinder containing steam with an impingement hood above
    - Combining conductive and convective drying

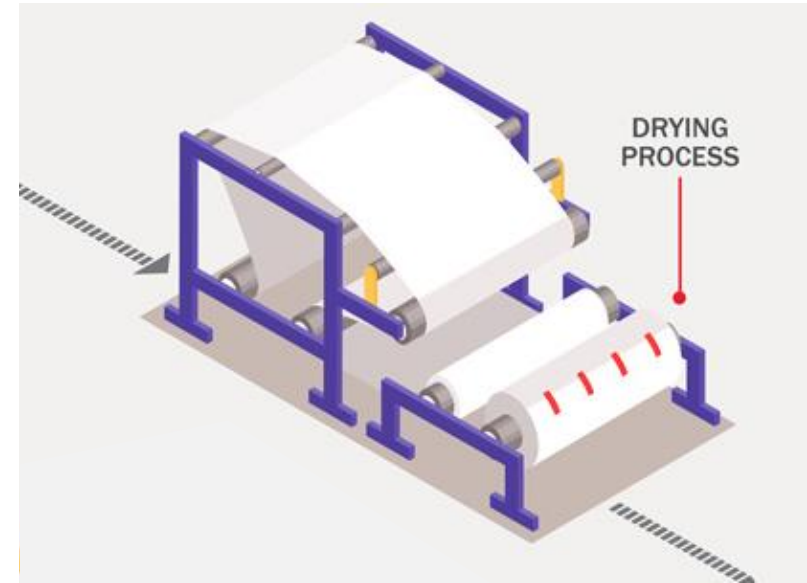


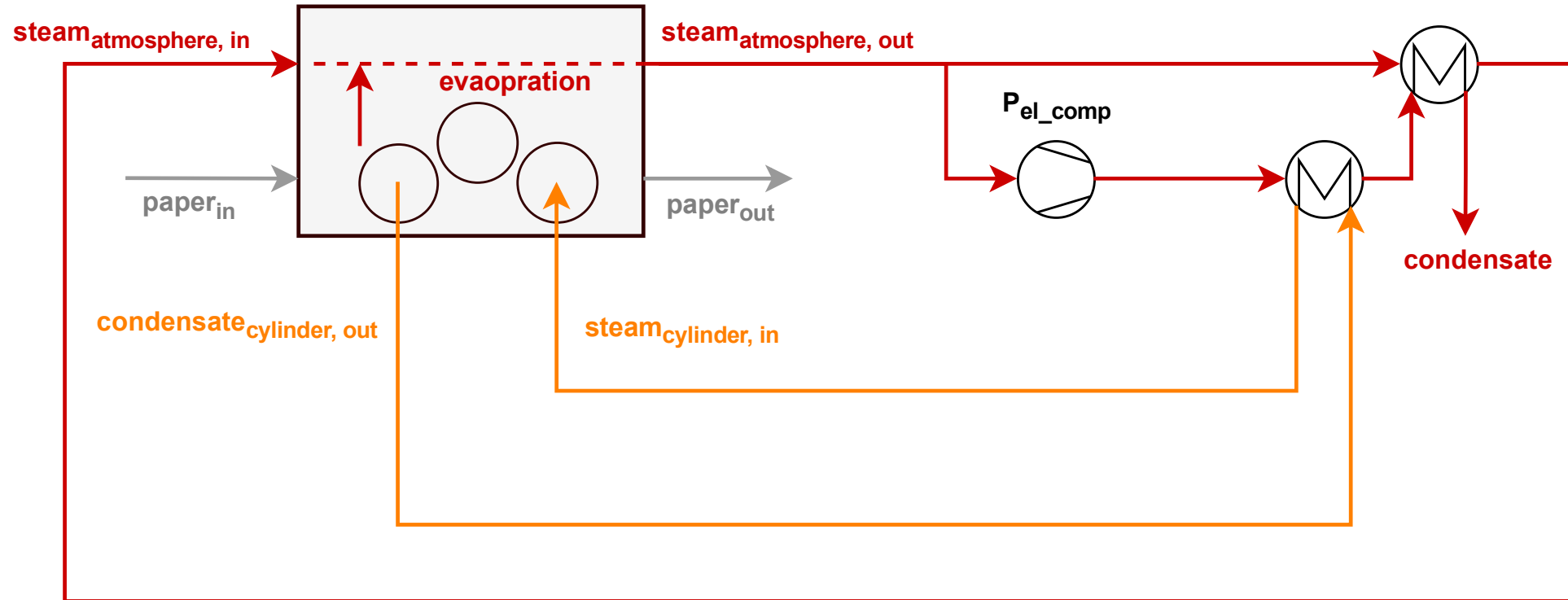
Image: Dwyer Instruments

# Multicylinder dryers (conductive drying)

- Multiple cylinders
  - Number depends on requirements/speed but in the order of 20-100 cylinders
- Cylinders are filled with saturated steam under pressure
  - Heat transfer to paper web mainly via cylinders (conduction)
- A hood with (pre-heated) air surrounding the cylinders
  - Mass transfer (evaporated water) via air in hood



# SHS drying concept for multicylinder dryers



AIT Austrian Institute of Technology, 2024



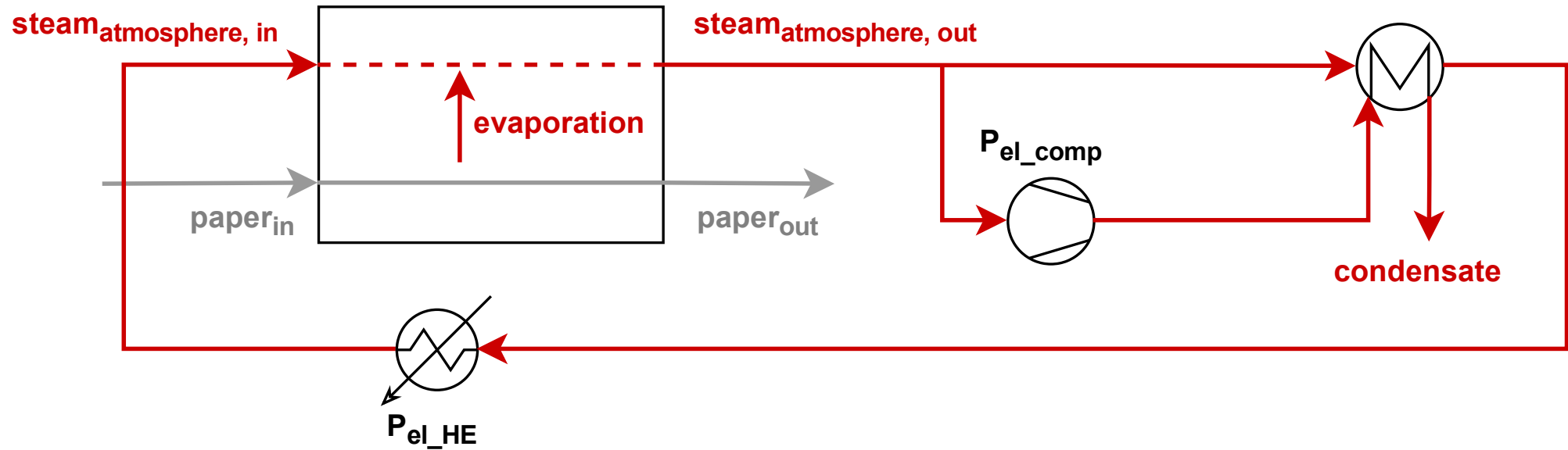
# Impingement dryer (convective drying)

- High-velocity and high-temperature
  - Air temperatures typically  $> 300^{\circ}\text{C}$
- Air jets focus directly on paper web, breaking the stagnant boundary layer
- Only convective heat transfer



OptiDry Curl impingement Valmet

# SHS drying concept for impingement dryer



AIT Austrian Institute of Technology, 2024

# What needs to be done?



Develop a pathway to superheat steam with electricity for a CO<sub>2</sub>-free drying process



Ensure high steam quality



Develop an advanced control system for SSD dryer (digital twin)



Pilot the SDD process for webs at relevant speeds (200 m/min)

# Challenge: Ensure high steam quality

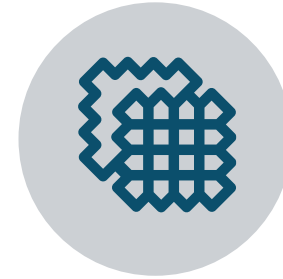
- With the SSD-technology steam is in direct contact with the paper web and will be recirculated
  - Risk of accumulation of contaminants:
    - Non-condensables entering the drying chamber
    - Dust/particles released from the fibre web
- Fouling needs to be kept at an acceptable level by
  - Prevention of dust and non-condensables entering the closed superheat steam loop
  - Removal of dust and non-condensables from the closed superheated steam loop

# Prevention



Non-condensables

- Proper sealing of the feeding and discharge of SSD to prevent air infiltration
- More difficult than for pulp and coal since paper is one continuous sheet



Dust

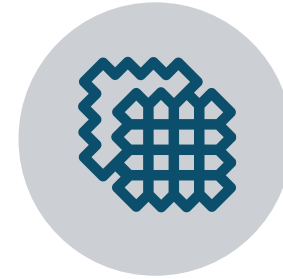
- Understand effect of steam flow on fibre release and adapt process where possible

# Removal



Non-condensables

- Separation of air/non-condensables from superheated steam
  - Hydrophobic membrane
  - Condensation



Dust

- Separation of dust from steam
  - Cyclones
  - Filters

Prevent condensation!

# Approach

The work on prevention and removal of dust and non-condensables is carried out by WFBR, UT and Valmet

- PhD student Ahmed Saleem (UT) works on understanding fibre-fibre interactions and release of fibres from the paper web. WFBR works on the experimental validation.
- PhD student Felipe de Oliveira (UT) works on cleaning the superheated steam both from dust and non-condensables
- Valmet together with WFBR investigate the sealing solutions to prevent air from entering the SSD

# Conclusions and Outlook

- SSD reduces energy consumption significantly when the steam is reused by:
  - Recirculation SHS
  - Recovery of latent heat from surplus steam
- Technology is not new → Industrial applications e.g. beet pulp and lignite coal
- High potential for SSD in paper industry → further developed in SteamDry
  - Develop and pilot technology
  - Ensure steam quality
- Other industries can also benefit from SSD
  - Drying of sensitive products
  - Microbial decontamination of foods



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Thank you  
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